

(19)



Europäisches Patentamt  
European Patent Office  
Office européen des brevets

(11) Publication number:

**0 324 528**  
**A1**

(12)

# EUROPEAN PATENT APPLICATION

(21) Application number: **89200070.4**(51) Int. Cl.4: **C10G 65/12**(22) Date of filing: **12.01.89**(30) Priority: **14.01.88 FR 8800360**(43) Date of publication of application:  
**19.07.89 Bulletin 89/29**(84) Designated Contracting States:  
**BE CH DE ES FR GB IT LI NL SE**(71) Applicant: **SHELL INTERNATIONALE  
RESEARCH MAATSCHAPPIJ B.V.**  
**Carel van Bylandtlaan 30**  
**NL-2596 HR Den Haag(NL)**(72) Inventor: **Lucien, Jacques**  
**Route de Caen**  
**F-76530 Grand Couronne(FR)**  
Inventor: **Dutot, Gilbert**  
**Route de Caen**  
**F-76530 Grand Couronne(FR)**(74) Representative: **Aalbers, Onno et al**  
**P.O. Box 302**  
**NL-2501 CH The Hague(NL)**(54) **Process for the preparation of a lubricating base oil.**

(57) Process for the preparation of a lubricating base oil with a high viscosity index and a low pour point by catalytic dewaxing, which process comprises contacting under dewaxing conditions a feedstock containing at least part of the hydrocrackate of a wax-containing mineral oil fraction, which feedstock has a kinematic viscosity at 100 °C of at most 10 mm<sup>2</sup>/s, with a dewaxing catalyst. The invention further provides a lubricating mineral base oil comprising hydrocarbons with a boiling point of at least 250 °C, and having a viscosity index of at least 125 and a pour point of at most -20 °C.

**EP 0 324 528 A1**

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## PROCESS FOR THE PREPARATION OF A LUBRICATING BASE OIL

The present invention relates to a process for the preparation of a lubricating base oil with a high viscosity and a low pour point.

Lubricating base oils are derived from various mineral crude oils by a variety of refining processes. Generally these refining processes are directed to obtaining a lubricating base oil with a suitable viscosity index. Other usual characteristics for lubricating base oils include pour point, boiling range and viscosity.

The preparation of high viscosity index lubricating base oils can be carried out as follows. A crude oil is separated by distillation at atmospheric pressure into a number of distillate fractions and a residue, known as long residue. The long residue is then separated by distillation at reduced pressure into a number of vacuum distillates and a vacuum residue known as short residue. From the vacuum distillate fractions lubricating base oils are prepared by refining processes. By these processes aromatics and wax are removed from the vacuum distillate fractions. From the short residue asphalt can be removed by known deasphalting processes. From the deasphalted oil thus obtained aromatics and wax can subsequently be removed to yield a residual lubricating base oil, known as bright stock. The wax obtained during refining of the various lubricating base oil fractions is designated as slack wax.

In GB-A-1,429,494 a process is disclosed in which high viscosity index lubricating base oils are prepared by catalytic hydrocracking of wax that is obtained in the dewaxing of a residual mineral oil, by separating the hydrocracked product into one or more light fractions and a residual fraction, and by dewaxing the residual fraction to form a lubricating base oil. The dewaxing was carried out using a mixture of solvents. The lubricating base oil obtained in the known process had a viscosity index of up to about 155.

The drawback of the known process resides in the fact that although the viscosity index of the product obtained is excellent, the pour point of the product is not altogether satisfactory for certain applications, such as for use as refrigerator oils. That means that at certain temperatures that are not satisfactorily low, some constituents of the lubricating base oil begin to solidify. These constituents are in particular the unbranched paraffinic molecules.

It has already been acknowledged in the art that the desires as to a low pour point and a high viscosity index are contradictory, and that a balance is to be sought between removing waxy paraffins thereby obtaining a desired low pour point, and retaining branched isoparaffins in the lubricating base oil, which contribute to a good viscosity index. For instance, in EP-A-225,053 a process is disclosed for the production of a lubricating base oil, referred to therein as lube stock or lubricating oil stock, which has a low pour point and a high viscosity index. This is said to be achieved by a two-step process, in which the intermediate product obtained after a first dewaxing step has a pour point of at least 6 °C above the target pour point, i.e. the pour point of the product obtained after the second dewaxing step. Although this reference alleges that lubricating oil stocks with low pour point and high viscosity index are attainable, it appears from the examples that when a high viscosity index (VI), e.g. above 135, is obtained the pour point is relatively high, e.g. about -6.7 °C, whereas when a really low pour point of about -20 °C is obtained the VI has a value of about 100 to 110. It is therefore apparent that the object set in the reference has not quite been achieved.

The present invention is directed towards the achievement of low pour point together with high viscosity index. Accordingly the present invention provides a process for the preparation of a lubricating base oil with a high viscosity index and a low pour point by catalytic dewaxing, which process comprises contacting under dewaxing conditions a feedstock containing at least part of the hydrocrackate of a wax-containing mineral oil fraction, which feedstock has a kinematic viscosity at 100 °C of at most 10 mm<sup>2</sup>/s, with a dewaxing catalyst. By a low pour point is understood a pour point below -20 °C as determined by ASTM D-97, and by high VI is understood a viscosity index above 125 as determined by ASTM D-567.

Catalytic dewaxing is a known process. In this respect reference is made to e.g. US-A-3,700,585 and EP-A-178,699. In catalytic dewaxing the feedstock to be dewaxed is suitably contacted with a dewaxing catalyst, preferably in the presence of hydrogen. Suitable catalysts that can be used as dewaxing catalysts include zeolitic catalysts. The catalytic dewaxing is preferably carried out in the presence of a zeolitic catalyst comprising at least one zeolite selected from the group consisting of ZSM-5, ZSM-11, ZSM-23, ZSM-35, ZSM-12, ZSM-38, ZSM-48, offretite, ferrierite, zeolite beta, zeolite theta, zeolite alpha and mixtures thereof. It is especially preferred to use a catalyst which comprises a composite crystalline aluminium silicate as described in EP-A-178,699. Such a crystalline aluminium silicate is obtainable by maintaining an aqueous starting mixture comprising one or more silicon compounds, one or more aluminium compounds, one or more compounds of metals of group 1a of the Periodic Table of the Elements (MX) and an organic nitrogen compound at an elevated temperature until a composite aluminium silicate has formed and subsequently separating the crystalline aluminium silicate from the mother liquor, wherein the various

compounds are present in the starting mixture within the following molar ratios:

RN :  $R_4NY$  = 6 - 3000, preferably 25 - 600, in particular 40 - 450,

$SiO_2$  :  $R_4NY$  = 200 - 10000, preferably 300 - 2000, in particular 450 - 1500,

$SiO_2$  :  $Al_2O_3$  = 60 - 250, preferably 65 - 200,

5  $SiO_2$  : MX < 10, and

$H_2O$  :  $SiO_2$  = 5 - 65, preferably 8 - 50,

RN representing a pyridine and  $R_4NY$  representing an organic quaternary ammonium compound.

10 RN preferably represents a compound selected from the group consisting of pyridine, alkyl pyridines and substituted-alkyl pyridines, and in particular represents pyridine. The substituent R in the quaternary ammonium compound is preferably an alkyl group in particular containing from 1 to 8 carbon atoms, and Y represents an anion. More preferably the compound  $R_4NY$  represents tetrapropyl ammonium hydroxide. For further details on the preparation of the composite crystalline aluminium silicate reference is made to EP-A-178,699.

15 The catalyst may further contain one or more hydrogenating metals from Groups 6b, 7b and 8 of the Periodic Table of the Elements or one or more compounds thereof. Of particular interest are the metals molybdenum, tungsten, chromium, iron, nickel, cobalt, platinum, palladium, ruthenium, osmium, rhodium and iridium. Platinum, palladium and nickel are especially preferred. The metals or their compounds may be deposited on the zeolites by means of any method for the preparation of catalysts known in the art, such as impregnation, ion-exchange or (co)precipitation.

20 The metal-loaded catalysts suitably comprise from 1 to 50 %wt, preferably from 2 to 20 %wt, of a non-noble metal of Group 6b, 7b and/or 8; noble metals of Group 8 are suitably present in the catalysts in an amount of from 0.001 to 5 %wt, preferably from 0.01 to 2 %wt, all percentages being based on the total catalyst.

25 The catalytic dewaxing is preferably carried out at a temperature of 200 to 450 °C, in particular from 250 to 400 °C, and at a space velocity of 0.1 to 5.0 kg/l.catalyst.h, in particular from 0.5 to 2.0 kg/l.h. When the dewaxing is carried out in the presence of hydrogen the hydrogen (partial) pressure is preferably from 10 to 200 bar, in particular from 30 to 150 bar and the hydrogen/feedstock ratio is preferably from 100 to 2000 NI/kg, in particular from 300 to 1000 NI/kg.

30 The product of the catalytic dewaxing may contain some relatively light products, i.e. products with a boiling point below 300-400 °C, e.g. below 370 °C. Suitably these products are separated from the dewaxed product, generally by distillation, to yield one or more light fractions and a lubricating base oil fraction. It is an advantage of the present invention that the yield on lubricating base oil is high. The complete effluent or the lubricating base oil fraction may conveniently be subjected to a hydrotreating step.

35 The said hydrotreating step is known in the art and may be carried out at known conditions. Suitable conditions include a temperature of 150 to 330 °C, a hydrogen (partial) pressure of 30 to 150 bar, a space velocity of 0.5 to 4.0 kg/l.h and a hydrogen/feedstock ratio of 100 to 2000 NI/kg. Suitable hydrotreating catalysts comprise nickel, cobalt, tungsten, molybdenum, platinum, palladium or mixtures thereof on a carrier, such as alumina, silica-alumina, silica, zirconia, zeolites and the like. The catalyst may further comprise fluorine, phosphorus and/or boron. Advantageously the hydrogen pressure in the hydrotreating 40 step is substantially the same as in the dewaxing step. The temperature, gas rate and space velocity can be selected by the person skilled in the art, suitably from the range given above.

The feedstock for the catalytic dewaxing is suitably a part of the hydrocrackate of a wax-containing mineral oil fraction. The hydrocrackate has conveniently been obtained by hydrocracking the wax-containing mineral oil fraction over a hydrocracking catalyst at a temperature of 360 to 420 °C, a hydrogen (partial) 45 pressure of 50 to 200 bar, a space velocity of 0.5 to 2.0 kg/l.catalyst.h and a  $H_2$ /mineral oil fraction ratio of 500 to 2000 NI/kg. The hydrocracking catalyst can be selected from any hydrocracking catalyst known in the art. Suitably the hydrocracking catalyst comprises a carrier and at least one hydrogenating metal or a compound thereof, which carrier has been selected from the group consisting of silica, alumina, silica-alumina and the faujasite-type zeolites. The most preferred faujasite-type zeolite is zeolite Y. The most 50 preferred hydrogenating metals are nickel, cobalt, tungsten and molybdenum and mixtures thereof, but platinum and/or palladium may also be used. The catalyst may further comprise fluorine and/or phosphorus and/or boron. When nickel, cobalt, molybdenum and/or tungsten are used as hydrogenating metal, they are preferably present in the form of their sulphides.

55 The starting materials for the hydrocracking step is a wax-containing mineral oil fraction. As is known in the art, wax consists essentially of paraffinic hydrocarbons which readily separate by crystallization when an oil fraction containing them is cooled. Conveniently wax includes those hydrocarbons which separate by crystallization when the oil fraction is cooled to a temperature which may be as low as -50 °C, suitably from -10 to -40 °C, either in the absence or presence of one or more solvents, such as a ketone (methyl ethyl

ketone, acetone) and an aromatic compound (benzene, toluene, naphtha). The wax-containing fraction to be used comprises at least 50% by weight of paraffinic hydrocarbons, conveniently from 50 to 95 %wt of wax, separated by cooling to a temperature which may be as low as -50 °C. Preferably the wax-containing fraction comprises at least 80% by weight of n-paraffins and i-paraffins. Suitably, the wax-containing fraction

5 is slack wax separated from the distillate and/or residual lubricating base oils, as described above. The hydrocrackate or at least the lubricating base oil fraction thereof may be passed directly to the catalytic dewaxing step. It may, however, be advantageous to subject the hydrocrackate or the lubricating base oil fraction thereof to a solvent dewaxing step first. In this way wax is produced that can be recycled to the hydrocracking step. The solvent-dewaxed hydrocrackate (fraction) is then used as feedstock for the

10 catalytic dewaxing step. The solvent dewaxing can be carried out as described in the above British patent GB-A-1,429,494, using a mixture of methyl ethyl ketone and toluene or a mixture of a different ketone and/or a different aromatic compound.

The present process enables the production of high VI lubricating base oils, having a low pour point. The person skilled in the art is now enabled for the first time to prepare very high VI lubricating mineral

15 base oils having very low pour points. Accordingly, the present process provides a lubricating mineral base oil comprising hydrocarbons with a boiling point of at least 250 °C, and having a viscosity index of at least 125 and a pour point of at most -20 °C, preferably of at most -30 °C. It is emphasized that the viscosity index and pour point are obtained in a lubricating base oil in the absence of additives. Due to the low pour point and high viscosity index the need for additives like VI improvers and pour point depressants is greatly

20 reduced. This is advantageous since apart from the fact that these additives are expensive, they also tend to degrade during the use of the lubricating oil composition in which they are present, thereby deteriorating the lubricating properties of the composition. Such a lubricating base oil is obtainable by a process as described above. The viscosity index of the lubricating base oil of the present invention may be as high as 160 and the

25 pour point may be as low as -75 °C. Conveniently, the lubricating base oils according to the present invention have a viscosity index of 130 to 150 and a pour point of -60 to -30 °C.

The lubricating base oil according to the present invention comprises mineral hydrocarbons with a

boiling point of at least 250 °C. Suitably the lubricating base oil comprises hydrocarbons which boil for at least 90 %wt at a temperature of at least 250 °C. More preferably the hydrocarbons boil for at least 90 %wt

30 at a temperature of at least 300 °C, and in particular of at least 370 °C. Such hydrocarbons are suitably obtained by distillation at atmospheric or reduced pressure from the effluent of the catalytic dewaxing step described hereinbefore.

The lubricating base oil according to the present invention has a high viscosity index, but this does not say very much about the actual viscosity thereof. The kinematic viscosity of the lubricating base oil may

35 range within wide limits, and is preferably from 1 to 10 mm<sup>2</sup>/s at 100 °C, more preferably from 1.5 to 9.5 mm<sup>2</sup>/s.

The present invention also relates to a lubricating oil composition comprising a mineral lubricating base oil containing hydrocarbons with a boiling point of at least 250 °C and having a viscosity index of at least 125 and a pour point of at most -20 °C, and one or more lubricating oil additives. Such additives include

40 optionally overbased detergents, such as alkaline earth metal sulphonates and carboxylates, in particular alkyl salicylates, dispersants, such as hydrocarbyl-substituted succinimides, and also foam inhibitors, corrosion inhibitors and anti-oxidants. Although the need for VI improvers and/or pour point depressants is reduced and addition thereof to the lubricating base oil is no longer required in many cases, the present invention also covers lubricating oil compositions that contain both a lubricating base oil according to the

45 invention and one or more pour point depressants and/or VI improvers.

The invention will be further illustrated by means of the following Examples.

## EXAMPLES

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In the experiments of the Examples a dewaxing catalyst was used which has been prepared in accordance with the procedure described in EP-A-178,699. The dewaxing catalyst used corresponded with the composite aluminium silicate denoted "composite silicate B" in the said European application. Hence the catalyst had a aluminium content of 1.06%wt. The X-ray diffraction pattern of the catalyst showed the

55 following lines:

d-space (Å)	I/I <sub>max</sub> (%)
11.10	50
9.97	25
3.85	100
3.81	69
3.74	41
3.71	59
3.64	37
3.52	16
3.44	22

Different feedstocks were used in the experiments, but they have all been obtained by hydrocracking slack waxes from different mineral crudes.

Feedstock A comprised the hydrocrackate of slack waxes and had the following characteristics: the kinematic viscosity at 100 °C ( $V_{k100}$ ) was 4.75 mm<sup>2</sup>/s; the pour point (ASTM D-97) was 42 °C; the initial boiling point was 350 °C and there was a 50% recovery at 449 °C. The wax content determined at -30 °C in the presence of methyl ethyl ketone (MEK)/toluene (1:1 volume ratio) was 31.1 %wt.

Feedstock B was a fraction of the hydrocrackate of slack wax which had been subjected to solvent dewaxing with a MEK/toluene mixture (1:1 volume ratio) at -22 °C, and which had the following characteristics:  $V_{k100}$  of 8.0 mm<sup>2</sup>/s and a pour point of -18 °C.

Feedstock C was a fraction of the hydrocrackate of slack waxes which had been subjected to a solvent dewaxing step like feedstock B but at a temperature of -26 °C. It had a  $V_{k100}$  of 5.4 mm<sup>2</sup>/s and a pour point of -18 °C.

Feedstock D was similar to Feedstock B and C, and had been solvent dewaxed at -26 °C, and had a  $V_{k100}$  of 4.2 mm<sup>2</sup>/s and a pour point of -21 °C.

Feedstock E was a fraction of a slack wax hydrocrackate having a  $V_{k100}$  of 6.27 mm<sup>2</sup>/s and a pour point of 38 °C. The initial boiling point was 345 °C, and 50 % was recovered at 480 °C. The wax content determined in the presence of a MEK/toluene mixture at -30 °C was 21.6 %wt.

Feedstock F was a fraction of the hydrocrackate of slack wax which had been subjected to solvent dewaxing with MEK/toluene at -22 °C. The  $V_{k100}$  was 5.60 mm<sup>2</sup>/s and the pour point was -16 °C.

#### EXAMPLE 1

The experiments of this Example have been carried out on feedstocks A to D in a 300 ml reactor loaded with the above dewaxing catalyst, diluted with 0.2 mm SiC particles in a 1:1 volume ratio. The experiments with solvent dewaxed feedstocks B, C and D employed a catalyst loaded with 0.2% by weight of palladium. The conditions under which the experiments have been carried out are indicated in Table I below. The product of the dewaxing was separated in a number of fractions and the fraction boiling at >370 °C was recovered as the desired lubricating base oil. The results of the experiments are indicated in Table I.

TABLE I

Experiment No.	1	2	3	4	5	6	7
Feedstock	A	B	C	C	D	D	D
Temperature, °C	380	380	400	380	360	360	340
WHSV, kg/l.h	1.0	0.8	1.0	1.0	1.0	1.0	1.0
H <sub>2</sub> pressure, bar	90	90	40	40	90	90	90
gas rate, NI H <sub>2</sub> /kg	700	700	700	700	700	700	700
YIELD, %wt on feedstock							
C <sub>1-4</sub>	51.2	54.0	26.9	29.2	20.8	29.1	24.0
C <sub>5-370</sub> °C	8.0	7.5	5.1	14.0	10.8	15.3	11.5
>370 °C	40.7	38.5	68.0	56.8	68.4	55.6	64.5
OIL PROPERTIES							
V <sub>k100</sub> , mm <sup>2</sup> /s	4.89	4.86	7.85	5.23	5.34	4.30	4.33
VI	127	125	135	127	130	126	130
pour point, °C	-42	-47	-36	-51	-40	-39	-33

From the above results it is apparent that the process according to the invention yields lubricating base oils with excellent pour points and VI's.

#### EXAMPLE 2

In the experiments of this Example two reactors were used in series, each of the size of the reactor used in Example 1. The first reactor was loaded with the dewaxing catalyst as in Example 1 loaded with 0.2% by weight palladium. The second reactor contained a hydrotreating catalyst comprising 2.5 %wt of nickel, 13.5 %wt of molybdenum and 2.9 %wt of phosphorus on alumina, the percentages being based on total catalyst. The operating conditions were: H<sub>2</sub> pressure of 90 bar, a gas rate of 700 NI H<sub>2</sub>/kg feedstock, and a space velocity, based on each reactor, of 1 kg/l/h. The temperatures in the reactors (T<sub>1</sub> and T<sub>2</sub>, respectively) and the results of the experiments are indicated in Table II.

TABLE II

Experiment No.	8	9	10	11	12
Feedstock	E	E	E	F	F
T <sub>1</sub> , °C	360	340	320	300	320
T <sub>2</sub> , °C	250	250	250	250	250
YIELD, %wt on feedstock					
C <sub>1-4</sub>	33.4	28.5	23.7	11.6	16.9
C <sub>5-370</sub> °C	6.0	9.1	8.9	7.5	7.4
>370 °C	60.6	62.4	67.4	80.9	75.7
OIL PROPERTIES					
V <sub>k100</sub> , mm <sup>2</sup> /s	6.26	6.37	6.34	5.87	5.87
VI	132	134	136	137	136
pour point, °C	-53	-44	-32	-30	-31

The above results show that excellent lubricating base oils can be obtained when the dewaxing process according to the invention is followed by a hydrotreating step.

## 5 Claims

1. Process for the preparation of a lubricating base oil with a high viscosity index and a low pour point by catalytic dewaxing, which process comprises contacting under dewaxing conditions a feedstock containing at least part of the hydrocrackate of a wax-containing mineral oil fraction which fraction comprises at least 50% by weight of paraffinic hydrocarbons, which feedstock has a kinematic viscosity at 100 °C of at most 10 mm<sup>2</sup>/s, with a dewaxing catalyst.

2. Process according to claim 1, which is carried out in the presence of a zeolitic catalyst comprising at least one zeolite selected from the group consisting of ZSM-5, ZSM-11, ZSM-23, ZSM-35, ZSM-12, ZSM-38, ZSM-48, offretite, ferrierite, zeolite beta, zeolite theta, zeolite alpha and mixtures thereof.

3. Process according to claim 1, which is carried out in the presence of a zeolitic catalyst comprising a composite crystalline aluminium silicate obtainable by maintaining an aqueous starting mixture comprising one or more silicon compounds, one or more aluminium compounds, one or more compounds of metals of Group 1a of the Periodic Table of the Elements (MX) and an organic nitrogen compound at an elevated temperature until a composite aluminium silicate has formed and subsequently separating the crystalline aluminium silicate from the mother liquor, wherein the various compounds are present in the starting mixture within the following molar ratios:

$$RN : R_4NY = 6 - 3000$$

$$SiO_2 : R_4NY = 200 - 10000$$

$$SiO_2 : Al_2O_3 = 60 - 250$$

$$SiO_2 : MX < 10, \text{ and}$$

$$H_2O : SiO_2 = 5 - 65,$$

RN representing a pyridine and R<sub>4</sub>NY representing an organic quaternary ammonium compound.

4. Process according to any one of claims 1-3, which is carried out at a temperature of 200 to 450 °C and at a space velocity of 0.1 to 5.0 kg/l.catalyst.h.

5. Process according to any one of the preceding claims, which is carried out in the presence of hydrogen.

6. Process according to claim 5, which is carried out at a hydrogen (partial) pressure of 10 to 200 bar and a hydrogen/feedstock ratio of 100 to 2000 NI/kg.

7. Process according to any one of claims 1-6, in which the dewaxing catalyst comprises one or more metals from the Groups 6b, 7b and 8 of the Periodic Table of the Elements or one or more compounds thereof.

8. Process according to any one of claims 1-7, in which the complete effluent or the lubricating base oil fraction of the product of the catalytic dewaxing is subjected to a hydrotreatment.

9. Process according to any one of claims 1-8, in which the feedstock has been obtained by hydrocracking the wax-containing mineral oil fraction over a hydrocracking catalyst at a temperature of 360 to 420 °C, a hydrogen (partial) pressure of 50 to 200 bar, a space velocity of 0.5 to 2.0 kg/l.catalyst.h and a H<sub>2</sub>/mineral oil fraction ratio of 500 to 2000 NI/kg.

10. Process according to claim 9, in which the hydrocracking catalyst comprises a carrier and at least one hydrogenating metal or a compound thereof, which carrier has been selected from the group consisting of silica, alumina, silica-alumina and the faujasite-type zeolites.

11. Process according to any one of claims 1-10, in which the wax-containing oil fraction contains from 50 to 95 %wt of wax, separated by cooling the mineral oil fraction to a temperature which may be as low as -50 °C.

12. Process according to any one of claims 1-11, in which the wax-containing mineral oil fraction comprises at least 80% by weight of n-paraffins and i-paraffins.

13. Lubricating mineral base oil comprising hydrocarbons with a boiling point of at least 250 °C, and having, in the absence of additives, a viscosity index of at least 125 and a pour point of at most -20 °C.

14. Lubricating mineral base oil according to claim 13 wherein the pour point is at most -30 °C.

15. Lubricating base oil according to claim 13 or 14, having a viscosity index of up to 160 and a pour point as low as -75 °C.

16. Lubricating base oil according to claim 15, having a viscosity index of 130 to 150 and a pour point of -60 to -30 °C.

17. Lubricating base oil according to any one of claims 13-16, comprising hydrocarbons which for at least 90 %wt boil at a temperature of at least 250 °C.

18. Lubricating base oil according to any one of claims 13-17, which has a kinematic viscosity at 100 °C of 1 to 10 mm<sup>2</sup>/s.

5 19. Lubricating base oil whenever prepared in a process according to any one of claims 1-12.

20. Lubricating oil composition comprising a lubricating base oil according to any one of claims 13-19 and one or more lubricating oil additives.

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DOCUMENTS CONSIDERED TO BE RELEVANT			
Category	Citation of document with indication, where appropriate, of relevant passages	Relevant to claim	CLASSIFICATION OF THE APPLICATION (Int. Cl.4)
X	EP-A-0 092 376 (MOBIL OIL) * Claims 1-12; example 3 *	1,2,4-20	C 10 G 65/12
Y	---	3	
D,Y	EP-A-0 178 699 (SHELL) * Claims *	3	
A	EP-A-0 185 448 (MOBIL OIL) * Claims 1-5 *	2	
			TECHNICAL FIELDS SEARCHED (Int. Cl.4)
			C 10 G
The present search report has been drawn up for all claims			
Place of search THE HAGUE		Date of completion of the search 03-03-1989	Examiner MICHIELS P.
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